

2054

B.E. (Mechanical Engineering)

Sixth Semester

MEC-604: Heat Transfer ✓

Time allowed: 3 Hours

Max. Marks: 50

**NOTE:** Attempt five questions in all, including Question No. 1 which is compulsory and selecting two questions from each Part.

x-x-x

- 1 a State the assumptions on which Fourier's law of conduction is based. 10  
 b Draw configurations of annular fin and straight rectangular fin.  
 c Differentiate between pool boiling and forced convection boiling.  
 d How are heat exchangers classified?  
 e State and explain Stefan-Boltzmann law.

## PART-A

- 2 Derive an expression for one dimensional time dependent heat conduction with internal heat generation and constant thermal conductivity in cartesian coordinate system. Reduce it as: 10  
 (i) Poisson equation,  
 (ii) Fourier equation,  
 (iii) Laplace equation.

- 2 a A hollow sphere of inside radius 30 mm and outside radius 50 mm is electrically heated at its inner surface at a constant rate of  $10^5 \text{ W/m}^2$ . The outer surface is exposed to a fluid at  $30^\circ\text{C}$ , with heat transfer coefficient of  $170 \text{ W/m}^2\cdot\text{K}$ . The thermal conductivity of the material is  $20 \text{ W/mK}$ . Calculate inner and outer surface temperatures. 5

- b Explain electrical analogy by considering Thermal resistance network for a hollow sphere subjected to convection heat transfer at inner and outer surfaces. 5

- 4 a If a thin and long fin, insulated at its tip is used, show that the heat transfer from the fin is given by 6

$$Q_{\text{fin}} = h P K A_c (T_0 - T_\infty) \tanh (mL)$$

Where symbols or variables in above equation are being used in their conventional or standard sense.

- b Write down temperature distribution and heat loss equations for fins of uniform cross-section (not derivation) 4  
 a) insulated tip b) infinitely long fin

## PART-B

- 5 a Using dimensional analysis, derive an expression for heat transfer coefficient in forced convection in terms of Nusselt number, Reynolds number and Prandtl numbers. 6

Contd.....P/2



(2)

- b Regarding the relative growth of velocity and thermal boundary layers in a fluid, how, for laminar conditions, thickness of thermal boundary layer is related to hydrodynamic boundary layer. 4
- 6 a The temperature of a body of area  $0.1 \text{ m}^2$  is  $900 \text{ K}$ . Calculate the total rate of energy emission, intensity of normal radiation in  $\text{W}/(\text{m}^2\text{sr})$ , maximum monochromatic emissive power, and wavelength at which it occurs. 7
- b What does the view factor represent? When is the view factor from a surface to itself not zero? 3
- 7 a Differentiate between film condensation and drop-wise condensation. In which case is the heat transfer higher? Why? 3
- b In a certain double pipe heat exchanger hot water flows at a rate of  $5000 \text{ kg/h}$  and gets cooled from  $95^\circ\text{C}$  to  $65^\circ\text{C}$ . At the same time  $50000 \text{ kg/h}$  of cooling water at  $30^\circ\text{C}$  enters the heat exchanger. The flow conditions are such that overall heat transfer coefficient remains constant at  $2270 \text{ W}/\text{m}^2 \text{ K}$ . Determine the heat transfer area required and the effectiveness, assuming two streams are in parallel flow. Assume for the both the streams  $C_p = 4.2 \text{ kJ}/\text{kg K}$ . 7

x-x-x