

2053

B.E. (Biotechnology) Fourth Semester  
BIO-413: Chemical Reaction Engineering

Time allowed: 3 Hours

Max. Marks: 50

**NOTE:** Attempt five questions in all, including Question No. 1 which is compulsory and selecting two questions from each Section.

x-x-x

1. Attempt the following:-

- a) Derive expressions for the overall conversions for a reaction of known order.
- b) Differentiate elementary and non-elementary reactions.
- c) What do you understand if the space time of a flow reactor is reduced?
- d) Express the most essential requisite for running a continuous reactor.
- e) Assuming any reactor operation, differentiate between competitive and non-competitive inhibition for an enzyme reaction.
- f) A simple autocatalytic reaction is represented by  $A+B \rightarrow B+B$ . starting with a small concentration of B, show in a plot how the rate will rise as B is formed.
- g) What is the relation between initial concentration ( $C_0$ ) and final concentration ( $C_4$ ) for a system of 4 equal sized mixed reactors in series? Assume reaction is of first order and  $t$  is the residence time.
- h) Define temperature dependency as per Arrhenius law.
- i) Deduce the expression for conversion for a variable density system.
- j) Enlist the kinetic models for the evaluation of non-elementary reactions.

(1x10)

**Section – A**

2. Distinguish between the methods available for establishing the kinetics of chemical reactions from the data obtained in a batch or continuous reactor. Give a brief account on determination of overall order of reaction from half-life method. (10)
3. A) Compare the performances and merits of the plug flow and the stirred tank reactors behaving ideally.  
B) A gaseous feed of pure A (2 mol/liter, 100 mol/min.) decomposes to give a variety of products in a plug flow reactor. The kinetics of conversion is represented as by  $A \rightarrow 2.5 \text{ Products}$ ,  $-r_A = (10 \text{ min}^{-1}) \cdot C_A$ . Find the expected conversion in 22-liter reactor. (4,6)

P.T.O.

(2)

4. An elementary reaction  $A \rightarrow R \rightarrow S$ , takes place in a mixed flow reactor. Find the condition for maximum concentration of R. What is its value? (Assume no R and S initially; Also  $k_1 = k_2$ ). (10)

**Section – B**

5. What is understood by 'optimum temperature progression'? Illustrate with an example of reversible exothermic reaction using a given feed material. (10)
6. a) An aqueous reactant stream (4 mol A/ liter) passes through a mixed flow reactor followed by a plug flow reactor. Find the concentration at the exit of the plug flow reactor if in the mixed flow reactor  $C_A = 1$  mol/liter. The reaction is second order with respect to A, and the volume of the plug flow unit is three times that of mixed flow unit.
- b) Illustrate which type of reactor would you choose for series reaction scheme  $A \rightarrow R \rightarrow S$  for different combinations of  $k_1$  and  $k_2$ . (6,4)
7. A) Discuss in details substrate limited cell-growth and the toxin limited cell-growth.  
B) Discuss the Monod's growth model for describing the kinetics of substrate utilization. (5,5)

x-x-x