Exam.Code:1032 Sub. Code: 7564

2123

M. E. (Bio-Technology) First Semester

ME-BIO-104: Bio-Separation and Bio-Process Technology

Time allowed: 3 Hours

Max. Marks: 50

NOTE: Attempt <u>five</u> questions in all, including Question No. I which is compulsory and selecting two questions from each Section. State clearly your assumptions.

x-x-x

1) Write briefly:

 $(2\times5=10)$

- a) Fermentation media.
- b) Sterilization.
- c) Precipitation.
- d) Yield coefficients.
- e) Upstream and downstream.

SECTION - A

2) Briefly discuss:

Centrifugation and design of centrifuge.

Filtration and different types of filters.

(5, 5)

3) Discuss the various methods of cell disruption with suitable examples.

(10)

- **4.A)** In a fermentation process producing baker's yeast, the biomass is separated using a continuous centrifuge, operating at 5000 rpm with a feed rate of 90 L/min. The solid particles may be assumed to have an average diameter of 0.05 mm. The density of the biomass is 1010 kg/m³. The fluid may be assumed to have properties of water. Find the sigma factor for the centrifuge.
 - B) Briefly discuss about electrophoresis?

(6, 4)

SECTION - B

5) Write a critical review on "Energy production or green chemical from biomass".

(10)

6) Suppose you have a microorganism that obeys the Monod equation:

$$\frac{dC_x}{dt} = \frac{\mu_{\text{max}} C_x C_x}{K_c + C_c}$$

where $\mu_{max} = 0.7 \text{ hr}^{-1}$ and $K_s = 5 \text{g/L}$. The Cell yield $(Y_{x/s})$ is 0.65. You want to cultivate this microorganism in either one reactor or two in series. The flow rate and Substrate concentration of the inlet stream should be 500 L/hr and 85 g/L, respectively. The substrate concentration of the outlet stream must be 5 g/L.

- a) If you use one CSTR, what should be the size of the Reactor? What is the cell concentration of the outlet stream?
- b) If you use two CSTR in series, what size of the two Reactors will be most productive? (10)
- 7.A) Discuss the bioreactor modeling of batch, fed batch and CSTR with cell mass, substrate and product balance. Explain merit and demerit of Batch, CSTR and fed batch reactor. (6)

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B) The specific growth rate for inhibited growth in chemostat is given by the following equation:

$$\mu = \frac{\mu_{\text{max}} S}{K_s + S + \frac{I.K_s}{K_I}}$$

Where $\mu_{max} = 0.5 \text{ hr}^{-1}$ and $K_s = 1.0 \text{ g/L}$, I = 0.05 g/L, $Y_{x/s} = 0.1 \text{ (g cells/g substrate)}$, $K_I = 0.01 \text{ g/L}$, S0 = 10 g/L, $X_0 = 0$

- a) Determine Cell mass (X) and substrate concentration as a function of D when I=0
- b) With inhibitor added to a chemostat determine Cell mass (X) and substrate concentration as a function of D.
- c) Determine Cell Productivity (DX) as a function of D.

(4)