1019

B.E. (Biotechnology) Fourth Semester BIO-412: Thermodynamics

Time allowed: 3 Hours

032

lse

de

er?

a

B

Im

a

I

Max. Marks: 50

 10×1

NOTE: Attempt <u>five</u> questions in all, including Question No. I which is compulsory and selecting two questions from each Section. Assume missing data, if any, reasonably.

x-x-x

- i. What is Gibbs phase rule for a nonreactive system?
- ii. Define activity coefficient.
- iii. Define partial molar properties.
- iv. What is chemical potential?
- v. What is enthalpy of a system? How is it related to internal energy?
- vi. When muscles contract, chemical energy is converted to mechanical energy with the loss of heat. Define the law of thermodynamics which this example represents.
- vii. Which molecule is considered to be the energy currency of cells?
- viii. What is inversion temperature?
- ix. Give examples of intensive and extensive properties.
- x. A container filled with a sample of an ideal gas at the pressure of 1.5 atm. The gas is compressed isothermally to one-fourth of its original volume. What is the new pressure of the gas?

Section A

II (a) If a gas of volume 6000 cm³ and at a pressure of 100 kPa is compressed 4 quasistatically according to PV^2 = constant, until the volume becomes 2000 cm³, determine the final pressure and the work transfer.

(b) 2 kilo mole of CO₂ occupies a volume of 0.380 m³ at 313 K. Calculate the 6 pressure using ideal gas equation and van der Waals equation. Take van der Waals constants to be $a = 0.365 \text{ Nm}^4/\text{mol}^2$ and $b = 4.28 \times 10^{-5} \text{ m}^3/\text{mol}$.

- (a) What is the principle of operation of an absorption refrigeration system?
 (b) Explain the Claude process for the liquefaction of air. Derive an expression 7 for the liquid yield obtained from the process.
- IV One mole of ideal gas, initially at 150°C and 8 bar pressure, undergoes the 10 following mechanically reversible changes: It expands isothermally to a pressure such that when it is cooled at constant volume to 50°C its final pressure is 3 bar. Calculate the work, heat transferred, changes in internal energy and changes in enthalpy for the process. Take $C_p = (7/2)R$ and $C_v = (5/2)R$.

Section B

-2-

(a) Initially n_0 moles of ammonia are present which dissociate according to the $\sqrt{27}$ (a) initially no mores of animona are provided in the equilibrium $K = \frac{\sqrt{27}}{4} \frac{\varepsilon^2}{1-\varepsilon^2} P$, equation $NH_3 \leftrightarrow \frac{1}{2} NH_2 + \frac{3}{2} H_2$. Show that at equilibrium $K = \frac{\sqrt{27}}{4} \frac{\varepsilon^2}{1-\varepsilon^2} P$. (b) The enthalpy of a binary liquid system for species 1 and 2 at fixed s Temperature (T) and pressure (P) is given by equation $H = x_1x_2 (40x_1 + 20x_2)$ where H is in J/mole. Determine expression for $\overline{H_1}$ and $\overline{H_2}$ as a function of x_1 and the numerical values for the partial enthalpies infinite at dilution \overline{H}_1 and \overline{H}_2

T

Λ

An equimolar mixture of $CH_4(g)$ and H_2O_2 (g) enters a reactor which is 10^{10} VI maintained at 1000K and 5 bar. The following reaction takes place

$$CH_4(g) + H_2O(g) \rightarrow CO(g) + 3H_2(g)$$

Calculate the equilibrium constant at 1000 K and estimate the degree of conversion of methane into products. Also estimate the composition of the reactor effluent assuming that the reaction mixture behaves like an ideal gas.

$$\begin{split} C_{p} &= a + bT + cT^{2} + dT^{3} + eT^{-2} (J/mol K), \\ \Delta H_{rxn}^{o} &= 206.408 \, kJ, \, \Delta G_{rxn}^{o} = 141.933 \, kJ \\ C_{p_{CO}} &= 28.068 + 4.631 \times 10^{-3}T - 0.258 \times 10^{5}T^{-2} \\ C_{p_{H_{2}}} &= 27.012 + 3.509 \times 10^{-3}T + 0.690 \times 10^{5}T^{-2} \\ C_{p_{CH_{4}}} &= 17.449 + 60.449 \times 10^{-3}T + 1.117 \times 10^{-6}T^{2} - 7.204 \times 10^{-9}T^{3} \\ C_{p_{H_{2}O}} &= 28.850 + 12.055 \times 10^{-3}T + 0.690 \times 10^{5}T^{-2} \end{split}$$

VII

V

Binary system Acetonitrile (1)/Nitromethane (2) conforms closely to Raoult's law. Vapor pressure for the pure species are given by the following Antoine 10

$$\ln P_1^{sat}(kPa) = 14.2724 - \frac{2945.47}{t({}^{0}C) + 224}$$
$$\ln P_2^{sat}(kPa) = 14.2043 - \frac{2972.64}{t({}^{0}C) + 209}$$

Prepare a t-x-y diagram for a pressure of 70kPa.

X-X-X